

This article was downloaded by:

On: 28 January 2011

Access details: *Access Details: Free Access*

Publisher *Taylor & Francis*

Informa Ltd Registered in England and Wales Registered Number: 1072954 Registered office: Mortimer House, 37-41 Mortimer Street, London W1T 3JH, UK



Physics and Chemistry of Liquids

Publication details, including instructions for authors and subscription information:

<http://www.informaworld.com/smpp/title~content=t713646857>

Evaluation of Excess Molar Volumes of n -butanol with nitrobenzene-aniline-acetonitrile Binary Liquid Mixtures at Temperatures of 298.15, 303.15, 308.15, and 313.15 K

M. A. Wahab^a; M. A. Islam^b; M. A. Ali^b; M. A. Mottaleb^c

^a Department of Polymer Science and Engineering, College of Engineering, Pusan National University, Pusan, South Korea ^b Department of Chemistry, Physical Chemistry Research Laboratory, University of Rajshahi, Rajshahi, Bangladesh ^c Environmental Science Division, National Exposure Research Laboratory, US Environmental Protection Agency, Las Vegas, NV, USA

Online publication date: 27 October 2010

To cite this Article Wahab, M. A. , Islam, M. A. , Ali, M. A. and Mottaleb, M. A.(2003) 'Evaluation of Excess Molar Volumes of n -butanol with nitrobenzene-aniline-acetonitrile Binary Liquid Mixtures at Temperatures of 298.15, 303.15, 308.15, and 313.15 K', *Physics and Chemistry of Liquids*, 41: 2, 189 – 195

To link to this Article: DOI: 10.1080/00319100307953

URL: <http://dx.doi.org/10.1080/00319100307953>

PLEASE SCROLL DOWN FOR ARTICLE

Full terms and conditions of use: <http://www.informaworld.com/terms-and-conditions-of-access.pdf>

This article may be used for research, teaching and private study purposes. Any substantial or systematic reproduction, re-distribution, re-selling, loan or sub-licensing, systematic supply or distribution in any form to anyone is expressly forbidden.

The publisher does not give any warranty express or implied or make any representation that the contents will be complete or accurate or up to date. The accuracy of any instructions, formulae and drug doses should be independently verified with primary sources. The publisher shall not be liable for any loss, actions, claims, proceedings, demand or costs or damages whatsoever or howsoever caused arising directly or indirectly in connection with or arising out of the use of this material.

EVALUATION OF EXCESS MOLAR VOLUMES OF *n*-BUTANOL WITH NITROBENZENE–ANILINE–ACETONITRILE BINARY LIQUID MIXTURES AT TEMPERATURES OF 298.15, 303.15, 308.15, AND 313.15 K

M.A. WAHAB^a, M.A. ISLAM^b, M.A. ALI^b and M.A. MOTTALEB^{c,*}

^a*Department of Polymer Science and Engineering, College of Engineering, Pusan National University, Pusan 609-735, South Korea;* ^b*Department of Chemistry, Physical Chemistry Research Laboratory, University of Rajshahi, Rajshahi 6205, Bangladesh;* ^c*Environmental Science Division, National Exposure Research Laboratory, US Environmental Protection Agency P.O. Box, 93478, Las Vegas, NV 89193-3478, USA*

(Received 10 November 2002)

The excess molar volumes (V_m^E) of binary liquid mixture defined here: *n*-butanol and nitrobenzene, *n*-butanol and aniline, and *n*-butanol and acetonitrile have been determined as a function of mole fraction of *n*-butanol at temperatures of 298.15, 303.15, 308.15, and 313.15 K by a calibrated bi-capillary pycnometer. The V_m^E were obtained as negative values over the entire composition range in the order of *n*-butanol + nitrobenzene, < *n*-butanol + aniline, and < *n*-butanol + acetonitrile systems. The negative magnitude of V_m^E suggests the presence of specific intermolecular interaction in the three liquid mixtures.

Keywords: Excess molar volumes; Binary liquid mixtures; *n*-butanol; Nitrobenzene; Aniline; Acetonitrile

INTRODUCTION

Over the past three decades, various efforts have been made in understanding the theoretical and practical importance of binary/ternary liquid mixtures [1–6]. The physicochemical analysis has been found to be a useful tool for getting sound information about the structure and interactions of various liquid–liquid binary/ternary mixtures. The physicochemical properties of binary/ternary liquid mixtures such as alcohols and hydrocarbons have drawn a considerable interest in experimental and theoretical aspects [7–9]. Physical properties including dipole moment, thermodynamic properties have been reported in the literatures [10,11]. Besides the theoretical importance, the knowledge of physicochemical properties of multi-component mixtures is indispensable for chemical process industries. Examples are the petroleum or petrochemical industry

*Corresponding author. E-mail: Mottaleb.Mohammad@epamail.epa.gov

where physicochemical processes are involved to handle the mixtures of hydrocarbons such as alcohols, aldehydes, ketones etc. Importantly, it is necessary to know the interaction between the components of mixtures for accurate designing of equipment.

To investigate the property of binary liquid mixtures, a framework was developed in our laboratory and some studies have been reported [12–16]. The present article describes the excess molar volumes of (x) *n*-butanol + (1- x_1) nitrobenzene, or $x + (1-x_1)$ aniline, or $x + (1-x_1)$ acetonitrile in obtaining the information of interaction of the liquid mixtures at temperatures of 298.15, 303.15, 308.15, and 313.15 K. This is a continuation of a previous investigation [16].

EXPERIMENTAL

Materials and Procedure

The compounds *n*-butanol (purity 99.5%, Merck), acetonitrile (purity 99%, Fluka), nitrobenzene (purity 99.5% Merck), and aniline (analytical grade, Metheson, USA, purity 99.5%), were used. The density of the pure components and binary mixtures was measured by calibrated bi-capillary pycnometer and the density measurement method was reported elsewhere [14,16]. Special attention was given to avoid the evaporation of solutions after preparation. The purity of the chemical was compared with the literature values [17–20] (Table I) and the obtained values showed a good agreement with reported values [11,16,19,20].

The V_m^E of different binary mixtures were calculated using equation (A):

$$V_m^E/(\text{cm}^3 \text{mol}^{-1}) = (x_1 M_1 + x_2 M_2)/\rho_m - x_1 M_1/\rho_1 - x_2 M_2/\rho_2 \quad (\text{A})$$

where M_1 and M_2 represent the molecular weights of components 1 and 2 respectively. The x_1 and x_2 are the mole fractions of 1 and 2 components having densities ρ_1 and ρ_2 , respectively. The density (ρ_m) is the experimentally observed density of the binary liquid mixtures. All measurements were carried out in a thermostatically controlled and well-stirred water-bath with a temperature accuracy of $\pm 0.01^\circ\text{C}$, read on a Beckmann thermometer.

RESULTS

The values of V_m^E were determined for the liquid mixtures: x *n*-butanol + (1- x_1) nitrobenzene, or $x + (1-x_1)$ aniline, or $x + (1-x_1)$ acetonitrile at temperatures of 298.15, 303.15, 308.15, and 313.15 K. The results are presented in Table II. The obtained V_m^E values

TABLE I Composition of density data (g cm^{-3}) between experimental and literature values at 298.15 K

<i>n</i> -Butanol		Nitrobenzene		Aniline		Acetonitrile	
Experimental	Literature	Experimental	Literature	Experimental	Literature	Experimental	Literature
0.8058	0.8060	1.2035	1.2037 ^a	1.0175	1.0175	0.7766	0.7766

^a Represents density data at 20°C.

TABLE II Excess molar volumes (V_m^E) of *n*-butanol with nitrobenzene–aniline–acetonitrile at different temperatures

Mole Fraction	Temperature (K)			
	298.15	303.15	308.15	313.15
System: <i>n</i> -butanol + (1- x_1) nitrobenzene				
0.1005	-0.2185	-0.2651	-0.3064	-0.3562
0.2008	-0.4008	-0.4325	-0.4759	-0.5382
0.3005	-0.5253	-0.5405	-0.5715	-0.6350
0.4006	-0.588	-0.6220	-0.6545	-0.7173
0.5001	-0.6275	-0.6614	-0.6987	-0.7578
0.6007	-0.6121	-0.6545	-0.6808	-0.7412
0.7009	-0.5719	-0.6224	-0.6499	-0.7027
0.8001	-0.4906	-0.5488	-0.5792	-0.6285
0.9001	-0.3179	-0.4031	-0.4273	-0.4796
A ₀	-2.4855	-2.5873	-2.7008	-2.9287
A ₁	-0.1761	-0.3009	-0.2869	-0.2050
A ₂	0.7897	-1.4813	-1.8095	-2.2268
A ₃	-0.8150	-0.9893	-0.8358	-0.9520
SD	±0.0045	±0.0153	±0.02073	±0.0265
System: <i>n</i> -butanol + (1- x_1) aniline				
0.1007	-0.1172	-0.1481	-0.1612	-0.1793
0.2003	-0.2063	-0.2421	-0.2775	-0.2878
0.3007	-0.3040	-0.3335	-0.3540	-0.3719
0.3998	-0.3782	-0.3789	-0.3899	-0.3959
0.5007	-0.3702	-0.3962	-0.4069	-0.4199
0.6006	-0.3493	-0.3706	-0.3821	-0.3899
0.7007	-0.2983	-0.3481	-0.3553	-0.3682
0.7998	-0.2113	-0.2552	-0.2664	-0.2923
0.8999	-0.1250	-0.1549	-0.1678	-0.1885
A ₀	-1.4594	-1.5224	-1.6793	-1.7565
A ₁	-0.0052	-0.0440	0.0232	0.0551
A ₂	0.2918	0.0136	-0.1660	-0.4610
A ₃	-0.0631	0.07940	0.0212	0.0287
SD	±0.0087	±0.01193	±0.00878	±0.0088
System: <i>n</i> -butanol + (1- x_1) acetonitrile				
0.1004	-0.1029	-0.1158	-0.1261	-0.1485
0.2001	-0.1760	-0.1996	-0.2263	-0.2493
0.3002	-0.2394	-0.2789	-0.3148	-0.3382
0.3999	-0.2854	-0.3373	-0.3569	-0.3711
0.4999	-0.3022	-0.3525	-0.3737	-0.3962
0.6005	-0.2891	-0.3399	-0.3656	-0.3870
0.7002	-0.2506	-0.2948	-0.318	-0.3482
0.8010	-0.1969	-0.2247	-0.2395	-0.2789
0.8999	-0.1166	-0.1257	-0.1673	-0.1789
A ₀	-1.1929	-1.4101	-1.5059	-1.6449
A ₁	-0.0592	-0.1088	0.1144	-0.1418
A ₂	0.0394	0.2049	-0.1333	-0.3348
A ₃	-0.0850	0.0560	-0.8048	0.3078
SD	±0.00482	±0.00501	±0.01938	±0.02256

were fitted with least square method to four parameters of Redlich and Kister [21] equation (B);

$$V_m^E/(\text{cm}^3\text{mol}^{-1}) = x_1(1 - x_1) \sum_{j=0}^3 (A_j(2x_1 - 1)^j) \tag{B}$$

The values of A_j obtained by a least square method are summarized in Table II.

DISCUSSION

A relationship between the excess molar volumes and the mole fraction of *n*-butanol has been determined for each constituent such as nitrobenzene, aniline, and acetonitrile mixture at temperatures of 298.15, 303.15, 308.15, and 313.15 K. The results are shown in Figs. 1–3 and similar graphical features can be seen at investigated temperatures with chosen component mixtures. That is, a negative slope is followed by a positive after a particular mole fraction of *n*-butanol. In Fig. 1, the V_m^E of *n*-butanol and nitrobenzene mixture decreases with increasing the concentration of *n*-butanol. When a mole fraction of *n*-butanol was reached at 0.5001, the V_m^E values become lowest in all temperatures. The lowest values were found to be determined as -0.6275 , -0.6614 , -0.6987 ,

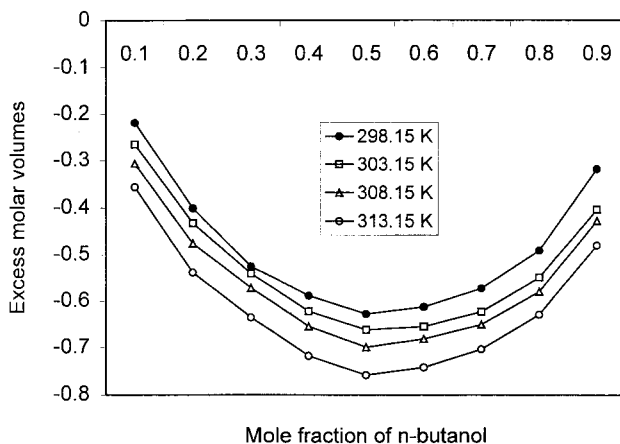


FIGURE 1 Effect of composition of mixture: *n*-butanol and nitrobenzene on excess molar volumes (V_m^E) at temperatures of 298.15, 303.15, 308.15, and 313.15 K.

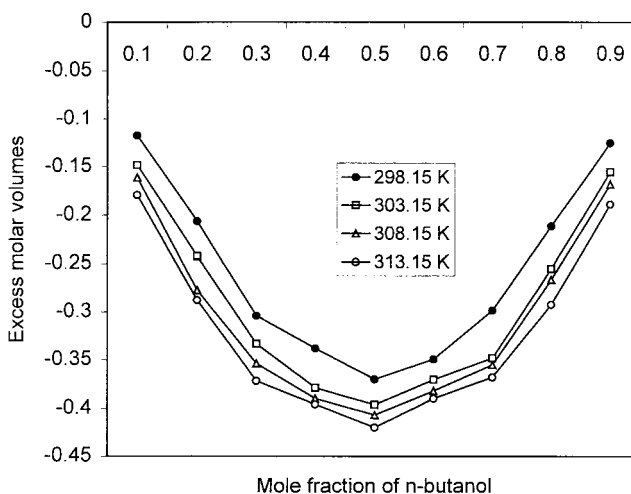


FIGURE 2 Effect of composition of mixture: *n*-butanol and aniline on excess molar volumes (V_m^E) at temperatures of 298.15, 303.15, 308.15, and 313.15 K.

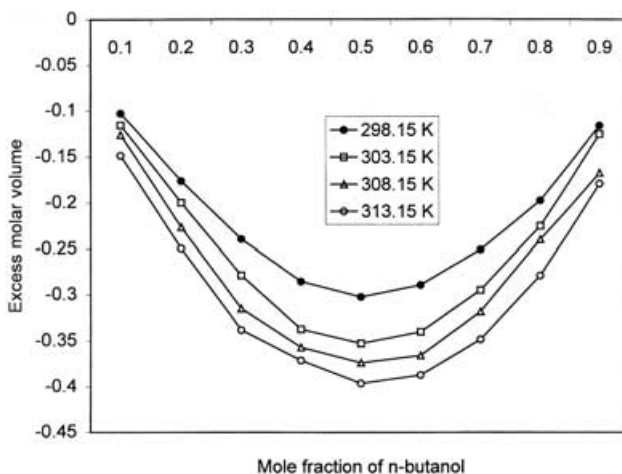
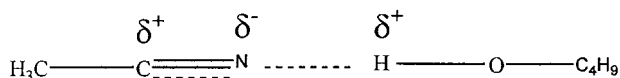


FIGURE 3 Effect of composition of mixture: *n*-butanol and acetonitrile on excess molar volumes (V_m^E) at temperatures of 298.15, 303.15, 308.15, and 313.15 K.

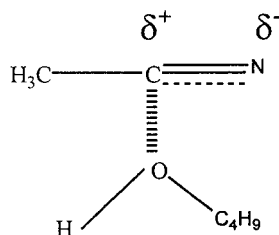
$-0.7578 \text{ cm}^3/\text{mol}$ at 298.15, 303.15, 308.15, and 313.15 K, respectively. An increment of the V_m^E was observed when the concentration of *n*-butanol was increased in the mixture and exceeded the minimum value. It was a common feature for all temperatures used. A similar result was observed for the *n*-butanol and aniline, and acetonitrile liquid mixtures (Figs. 2 and 3). The values of V_m^E decrease with increasing the mole fraction of *n*-butanol. The lowest values of V_m^E were found at 0.5007 and 0.4999-mole fraction when the aniline and acetonitrile were used, respectively. However, the lowest values of V_m^E in the *n*-butanol and aniline system, were determined as -0.3702 , -0.3962 , -0.4069 , and $-0.4199 \text{ cm}^3/\text{mol}$ at 298.15, 303.15, 308.15, and 313.15 K, respectively. For the *n*-butanol and acetonitrile mixture, the minimum V_m^E values were -0.3022 , -0.3525 , -0.3737 and $-0.3962 \text{ cm}^3/\text{mol}$ at 298.15, 303.15, 308.15, and 313.15 K, respectively.

According to Fort and Moore [22], a negative excess volume is an indication of strong heteromolecular interaction in the liquid mixtures and is attributed to charge-transfer, dipole-dipole, dipole-induced-dipole interactions and hydrogen bonding between the unlike components, while a positive sign indicates a weak interaction and is attributed to dispersive force (London forces), which are likely to be operative in every cases. The magnitudes of the contributions made by the different types of interactions will vary with the components and composition of the mixtures. In the present investigation, however, all the three mixtures gave negative magnitude of V_m^E , consistent with the presence of heteromolecular interaction in all the binary liquid mixtures, as indicated by the Fort and Moore observation.

Considering the *n*-butanol and acetonitrile mixture, it is probable that the interaction existing in the mixture is due to the formation of intermolecular hydrogen bonding between the cyano group ($-\text{CN}$) of acetonitrile and the hydroxyl group ($-\text{OH}$) of *n*-butanol. The hydrogen bonding interaction in the *n*-butanol with acetonitrile is as shown below:



It is probable that there is a dipole–dipole interaction in the *n*-butanol between the carbon atom of cyano group and the oxygen atom of hydroxyl group as shown below;



The dipole moments of the investigated *n*-butanol, nitrobenzene, aniline, and acetonitrile constituents are 1.63, 3.90, 1.53, and 3.0, respectively. Overall, the V_m^E (Figs. 1–3) for *n*-butanol and nitrobenzene, *n*-butanol and aniline, and *n*-butanol and acetonitrile mixtures can be explained in terms of (i) dipole–dipole interaction between the polar components and (ii) steric effect. The negative values of V_m^E of *n*-butanol + nitrobenzene and *n*-butanol + acetonitrile (Figs. 1 and 3) may be attributed to the breaking of self association existing in the pure liquids and the formation of hetero-association among the molecules of binary mixtures, where the latter is predominant. The partial accommodation of linear *n*-butanol molecule in between the interstitial spaces of the cyclic nitrobenzene and *n*-butanol + acetonitrile mixtures of specific interaction due to high polarity of the second components results in the decrease of the molar volumes of the mixtures. The excess molar volumes *versus* mole fraction of *n*-butanol curves (Figs. 1 and 3) showed a general agreement of shape with reported works for different mixtures such as butanol and benzene [23], toluene and aniline, water and aniline, *n*-hexane and aniline [11], and toluene and acetonitrile, and toluene and nitrobenzene [16]. In Fig. 2, the dipole moments of the components molecules are not very different, and the specific interaction between the unlike molecules are not unexpected. However, partial accommodation of the *n*-butanol molecule in between the aniline molecule may lead to decrease in the molar volume of the mixtures. It is also a fact for all mixtures that the creation of order would produce the negative V_m^E values. This interpretation can be applied to all the mixtures investigated in this study. The negative V_m^E values displayed by all the mixtures indicate a more ordered structure in solution. The negative values showed by all the mixtures were increased as the temperature increased. It suggests that interaction of components of solution was increased with increasing the temperatures.

CONCLUSIONS

The V_m^E from the densities data have been evaluated for binary mixtures of *n*-butanol with nitrobenzene, aniline, acetonitrile at four temperatures; 298.15, 303.15, 308.15, and 313.15 K. Analyses suggest the presence of a strong intermolecular interaction in all binary mixtures, which may be due to the dipole–dipole interaction between polar components, steric effects, and specific interaction between unlike molecules. The strength of intermolecular interaction increases with rise in temperatures.

References

- [1] O.K. Rice (1949). *Chem. Rev.*, **44**, 69.
- [2] G. Scotchard (1949). *Chem. Rev.*, **44**, 7.
- [3] J.H. Hildebrand (1949). *Chem. Rev.*, **44**, 37.
- [4] R.H. Stokes and K.H. Marsh (1972). *Ann. Rev. Phys. Chem.*, **23**, 65.
- [5] Y.S. Kian, J.K. Gerritaa and N.Y. Noore (1967). *Thermophysical Properties Research Literature Retrieval Guide*. Plenum Press, New York.
- [6] J.B. Irving (1967). NEL Report. No. 630 and 631, East Kilbridge, Glasgow.
- [7] A.J. Tresczanomic and G.C. Benson (1978). *J. Chem. Thermody.*, **10**, 967.
- [8] M.K. Kumaran and G.C. Benson (1983). *J. Chem Thermody.*, **15**, 245.
- [9] X.R. Rajkumar, K.V. Raman and S.T. Arulraj (1984). *Ind. J. Pure Appl. Phys.*, **22**, 241.
- [10] C. Berro and M.C. Angula (1984). *Chem. Eng. Data.*, **29**, 340.
- [11] M.A. Ali (1985). Ph.D. Thesis, Punjab University, Chandigar, India.
- [12] M.L. Lakhanpal and M.A. Ali (1987). *Ind. J. Chem.*, **26**, 648.
- [13] M.A. Ali, R. Prashar, A. Sharma and M.L. Lakhanpal (1989). *Ind. J. Chem.*, **28**, 512.
- [14] M.A. Ali and M.H. Rahman (1992). *J. Bang. Chem. Soc.*, **5**, 109.
- [15] R. Prashar, M.A. Ali and S.K. Metha (2000). *J. Chem. Thermody.*, **32**, 711.
- [16] M.A. Wahab, M.A. Ali and M.A. Mottaleb (2002). *Bull. Kor. Chem. Soc.* **23**, 953.
- [17] R.C. Weast (1975–76). *Handbook of Chemistry and Physics*, 5th Edn. CRC Press Inc., Boca Raton, Florida.
- [18] J.A. Riddick, W.B. Bunger and T.R. Sanako (1986). *Organic Solvent, Physical Properties and Methods of Purification*, 4th Edn. Wiley-Interscience, NY.
- [19] A. Das, M. Frenkel, N.M. Gadalla, K. Marsh and R.C. Wilhoit (1994). Thermodynamics Tables Texas Engineering Experimental Station, Texas A and M University System, College Station, TX.
- [20] Proc. Natl. Sci. Council. (2001). *ROC (A)*, **25**, 205.
- [21] O. Redlich and A.T. Kister (1948). *Ind. Eng. Chem.*, **40**, 345 equation.
- [22] R.T. Fort and W.R. Moore (1966). *Trans Faraday Soc.*, **62**, 1112.
- [23] B. Luca, C. Norberto, C. Giovanni, P. Gianni, M. Vincenzo, R.T. Naria, L. Luciano, M. Enrico and S. Andrea (2001). *J. Chem. Thermody.*, **33**, 629.